CHAPTER 29

REFRIGERANTS

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REFRIGERANTS are the working fluids in refrigeration, airconditioning, and heat-pumping systems. They absorb heat from one area, such as an air-conditioned space, and reject it into another, such as outdoors, usually through evaporation and condensation, respectively. These phase changes occur both in absorption and mechanical vapor compression systems, but not in systems operating on a gas cycle using a fluid such as air. (See Chapter 2 for more information on refrigeration cycles.) The design of the refrigeration equipment depends strongly on the selected refrigerant's properties. Tables 1 and 2 list standard refrigerant designations, some properties, and safety classifications from ASHRAE *Standard* 34.

Refrigerant selection involves compromises between conflicting desirable thermophysical properties. A refrigerant must satisfy many requirements, some of which do not directly relate to its ability to transfer heat. Chemical stability under conditions of use is an essential characteristic. Safety codes may require a nonflammable refrigerant of low toxicity for some applications. Environmental consequences of refrigerant leaks must also be considered. Cost, availability, efficiency, and compatibility with compressor lubricants and equipment materials are other concerns.

Latent heat of vaporization is another important property. On a molar basis, fluids with similar boiling points have almost the same latent heat. Because compressor displacement is defined on a volumetric basis, refrigerants with similar boiling points produce similar refrigeration effect with a given compressor. On a mass basis, latent heat varies widely among fluids. Efficiency of a theoretical vapor compression cycle is maximized by fluids with low vapor heat capacity. This property is associated with fluids having a simple molecular structure and low molecular mass.

Transport properties (e.g., thermal conductivity and viscosity) affect performance of heat exchangers and piping. High thermal conductivity and low viscosity are desirable.

No single fluid satisfies all the attributes desired of a refrigerant; consequently, various refrigerants are used. This chapter describes the basic characteristics of various refrigerants, and Chapter 30 lists thermophysical properties.

REFRIGERANT PROPERTIES

Global Environmental Properties

Chlorofluorocarbons (CFCs) and hydrochlorofluorocarbons (HCFCs) can affect both stratospheric ozone and climate change, whereas hydrofluorocarbons (HFCs) can affect climate change. Minimizing all refrigerant releases from systems is important not only because of environmental impacts, but also because charge losses lead to insufficient system charge levels, which in turn results in suboptimal operation and lowered efficiency.

Stratospheric Ozone Depletion. The stratospheric ozone layer filters out the UV-B portion of the sun's ultraviolet (UV) radiation. Overexposure to this radiation increases the risk of skin cancer,

cataracts, and impaired immune systems. It also can damage sensitive crops, reduce crop yields, and stress marine phytoplankton (and thus human food supplies from the oceans). In addition, exposure to UV radiation degrades plastics and wood.

Stratospheric ozone depletion has been linked to the presence of chlorine and bromine in the stratosphere. Chemicals with long atmospheric lifetimes can migrate to the stratosphere, where the molecules break down from interaction with ultraviolet light or through chemical reaction. Chemicals such as CFCs and HCFCs release chlorine, which reacts with stratospheric ozone.

Ozone-depleting substances, including CFCs and HCFCs, are to be phased out of production under the Montreal Protocol (UNEP 2003, 2006). U.S. regulations for CFC and HCFC refrigerants, including phaseout schedules, may be found at http://www.epa.gov/ozone/strathome.html. The Alliance for Responsible Atmospheric Policy (http://www.arap.org/regs/) also briefly summarizes regulations for several countries. Reclaimed CFC and HCFC refrigerants that meet the requirements of ARI *Standard* 700 can continue to be used for servicing existing systems.

Global Climate Change. The average global temperature is determined by the balance of energy from the sun heating the earth and its atmosphere and of energy radiated from the earth and the atmosphere to space. Greenhouse gases (GHGs), such as carbon dioxide ($\rm CO_2$) and water vapor, as well as small particles trap heat at and near the surface, maintaining the average temperature of the Earth's surface about 34 K warmer than would be the case if these gases and particles were not present (the greenhouse effect).

Global warming (also called global climate change) is a concern because of an increase in the greenhouse effect from increasing concentrations of GHGs attributed to human activities. The major GHG of concern is CO_2 released to the atmosphere when fossil fuels (coal, oil, and natural gas) are burned for energy. Methane (CH₄), nitrous oxide (N₂O), CFCs, HCFCs, HFCs, perfluorocarbons (PFCs), and sulfur hexafluoride (SF₆) are also GHGs.

In 1988, the United Nations Environment Programme (UNEP) and the World Meteorological Organization (WMO) established the Intergovernmental Panel on Climate Change (IPCC) to provide an objective source of information about the causes of climate change, its potential environmental and socioeconomic consequences, and the adaptation and mitigation options to respond to it. According to IPCC (2007a), atmospheric concentration of carbon dioxide has increased by more than 35% over the past 250 years, primarily from burning fossil fuels, with some contribution from deforestation. Concentration of methane has increased by over 145%, and nitrous oxide by about 18%. IPCC (2007a) deems atmospheric concentrations of fluorochemicals, including fluorocarbon gases (CFCs, HCFCs, and HFCs) and sulfur hexafluoride, to be a smaller contributor to global climate change. On whether observed warming is attributable to human influence, IPCC (2007b) concludes that "Most of the observed increase in global averaged temperatures since the mid-twentieth century [about 0.65 K] is very likely [90% confident] due to the observed increase in anthropogenic greenhouse gas concentrations."

The preparation of this chapter is assigned to TC 3.1, Refrigerants and Secondary Coolants.

Table 1 Refrigerant Data and Safety Classifications

	Table 1 Ref	frigerant Data and Safety Classifica	itions		
Refrigerar Number	nt Chemical Name ^{a,b}	Chemical Formula ^a	Molecular Mass ^a	Normal Boiling Point, ^a °C	Safety Group
Methane S	Series				
11	Trichlorofluoromethane	CCl ₃ F	137.4	24	A1
12	Dichlorodifluoromethane	CCl_2F_2	120.9	-30	A1
12B1	Bromochlorodifluoromethane	CBrClF ₂	165.4	<u>-4</u>	4.1
13	Chlorotrifluoromethane	CCIF ₃	104.5	-81 128	A1
14	Tetrafluoromethane (carbon tetrafluoride) Dichlorofluoromethane	CF ₄	88.0	-128	A1
21 22	Chlorodifluoromethane	CHCl ₂ F CHClF ₂	102.9 86.5	9	B1 A1
23	Trifluoromethane	CHF ₃	70.0	-82	A1
30	Dichloromethane (methylene chloride)	CH ₂ Cl ₂	84.9	-82 40	B2
31	Chlorofluoromethane	CH ₂ Cl ₂ CH ₂ ClF	68.5	_9	D2
32	Difluoromethane (methylene fluoride)	CH ₂ F ₂	52.0	-52	A2
40	Chloromethane (methyl chloride)	CH ₃ Cl	50.4	-24	B2
41	Fluoromethane (methyl fluoride)	CH ₃ F	34.0	-78	
50	Methane	CH_4	16.0	-161	A3
Ethane Se	ries	•			
113	1,1,2-trichloro-1,2,2-trifluoroethane	CCl ₂ FCClF ₂	187.4	48	A1
114	1,2-dichloro-1,1,2,2-tetrafluoroethane	CCIF ₂ CCIF ₂	170.9	4	A1
115	Chloropentafluoroethane	CCIF ₂ CF ₃	154.5	-39	A1
116	Hexafluoroethane	CF ₃ CF ₃	138.0	-78	A1
123	2,2-dichloro-1,1,1-trifluoroethane	CHCl ₂ CF ₃	153.0	27	B1
124	2-chloro-1,1,1,2-tetrafluoroethane	CHClFCF ₃	136.5	-12	A1
125	Pentafluoroethane	CHF_2CF_3	120.0	-79	A1
134a	1,1,1,2-tetrafluoroethane	CH_2FCF_3	102.0	-26	A1
141b	1,1-dichloro-1-fluoroethane	CH ₃ CCl ₂ F	117.0	32	
142b	1-chloro-1,1-difluoroethane	CH ₃ CCIF ₂	100.5	-10	A2
143a	1,1,1-trifluoroethane	CH ₃ CF ₃	84.0	-47 2.5	A2
152a	1,1-difluoroethane	CH ₃ CHF ₂	66.0	-25	A2
170	Ethane	CH ₃ CH ₃	30.0	-89	A3
Ethers E170	Dimethyl ether	CH ₃ OCH ₃	46.0	-25	A3
Propane S					
218	Octafluoropropane	$CF_3CF_2CF_3$	188.0	-37	A1
236fa	1,1,1,3,3,3-hexafluoropropane	CF ₃ CH ₂ CF ₃	152.0	-1	A1
245fa	1,1,1,3,3-pentafluoropropane	CF ₃ CH ₂ CHF ₂	134.0	15	B1
290	Propane	$CH_3CH_2CH_3$	44.0	-42	A3
Cyclic Org C318	ganic Compounds (see Table 2 for blends) Octafluorocyclobutane	-(CF ₂) ₄ -	200.0	-6	A1
	eous Organic Compounds	(C1 2)4	200.0	O	111
Hydroca	•				
600	Butane	CH ₃ CH ₂ CH ₂ CH ₃	58.1	0	A3
600a	Isobutane	CH(CH ₃) ₂ CH ₃	58.1	-12	A3
601	Pentane	$CH_3(CH_2)_3CH_3$	72.15	36.1	A3
601a	Isopentane	(CH ₃) ₂ CHCH ₂ CH ₃	72.15	27.8	A3
Oxygen	Compounds	, 3,2 2 3			
610	Ethyl ether	CH ₃ CH ₂ OCH ₂ CH ₃	74.1	35	
611	Methyl formate	$HCOOCH_3$	60.0	32	B2
	ompounds				
620	(Reserved for future assignment)				
	Compounds	A		_	
630	Methyl amine	CH ₃ NH ₂	31.1	_7 17	
631	Ethyl amine	$CH_3CH_2(NH_2)$	45.1	17	
	c Compounds	11	2.0	252	A 2
702 704	Hydrogen	H_2	2.0 4.0	-253 260	A3
704 717	Helium Ammonia	He NH ₃	4.0 17.0	-269 -33	A1 B2
717	Water	H_2O	18.0	-33 100	A1
720	Neon	Ne	20.2	-246	A1
728	Nitrogen	N ₂	28.1	-240 -196	A1
732	Oxygen	O_2	32.0	-183	111
740	Argon	O_2	39.9	-186	A1
744	Carbon dioxide	CO_2	44.0	-78°	A1
744A	Nitrous oxide	N_2O	44.0	-90	
764	Sulfur dioxide	SO_2	64.1	-10	B1
	ated Organic Compounds	2-2			
1150	Ethene (ethylene)	$CH_2=CH_2$	28.1	-104	A3
1270	Propene (propylene)	$CH_3CH=CH_2$	42.1	-48	A3
		J 4			

Source: ANSI/ASHRAE Standard 34-2007.

^aChemical name, chemical formula, molecular mass, and normal boiling point are not part of this standard.

^bPreferred chemical name is followed by the popular name in parentheses.

 $^{^{}c}Sublimes. \\$

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Table 2 Data and Safety Classifications for Refrigerant Blends

Refrigerant Number	Composition (Mass %)	Composition Tolerances	Azeotropic Temperature, °C	Molecular Normal Boiling Mass ^a Point, °C	Safety Group
Zeotropes					
400	R-12/114 (must be specified)		none		A1
	R-22/152a/124 (53.0/13.0/34.0)	$(\pm 2/\pm 0.5, -1.5/\pm 1)$			A1
401B	R-22/152a/124 (61.0/11.0/28.0)	$(\pm 2/\pm 0.5, -1.5/\pm 1)$			A1
401C	R-22/152a/124 (33.0/15.0/52.0)	$(\pm 2/\pm 0.5, -1.5/\pm 1)$			A1
402A	R-125/290/22 (60.0/2.0/38.0)	$(\pm 2/\pm 0.1, -1/\pm 2)$			A1
402B	R-125/290/22 (38.0/2.0/60.0)	$(\pm 2/\pm 0.1, -1/\pm 2)$			A1
403A	R-290/22/218 (5.0/75.0/20.0)	$(\pm 0.2, -2/\pm 2/\pm 2)$			A1
403B	R-290/22/218 (5.0/56.0/39.0)	$(\pm 0.2, -2/\pm 2/\pm 2)$			A1
404A	R-125/143a/134a (44.0/52.0/4.0)	$(\pm 2/\pm 1/\pm 2)$			A1
405A	R-22/152a/142b/C318 (45.0/7.0/5.5/42.5)	$(\pm 2/\pm 1/\pm 1/\pm 2)$			
406A	R-22/600a/142b (55.0/4.0/41.0)	$(\pm 2/\pm 1/\pm 1)$			A2
407A	R-32/125/134a (20.0/40.0/40.0)	$(\pm 2/\pm 2/\pm 2)$			A1
407B	R-32/125/134a (10.0/70.0/20.0)	$(\pm 2/\pm 2/\pm 2)$			A1
407C	R-32/125/134a (23.0/25.0/52.0)	$(\pm 2/\pm 2/\pm 2)$			A1
407D	R-32/125/134a (15.0/15.0/70.0)	$(\pm 2/\pm 2/\pm 2)$			A1
407E	R-32/125/134a (25.0/15.0/60.0)	$(\pm 2, \pm 2, \pm 2)$			A1
408A	R-125-143a-22 (7.0/46.0/47.0)	$(\pm 2/\pm 1/\pm 2)$			A1
409A	R-22/124/142b (60.0/25.0/15.0)	$(\pm 2/\pm 2/\pm 1)$			A1
409B	R-22/124/142b (65.0/25.0/10.0)	$(\pm 2/\pm 2/\pm 1)$			A1
410A	R-32/125 (50.0/50.0)	(+0.5, -1.5/+1.5, -0.5)			A1
	R-32/125 (45.0/55.0)	$(\pm 1/\pm 1)$			A1
411A	R-1270/22/152a (1.5/87.5/11.0)	(+0,-1/+2,-0/+0,-1)			A2
411B	R-1270/22/152a (3.0/94.0/3.0)	(+0,-1/+2,-0/+0,-1)			A2
412A	R-22/218/142b (70.0/5.0/25.0)	$(\pm 2/\pm 1/\pm 1)$			A2
413A	R-218/134a/600a (9.0/88.0/3.0)	$(\pm 1/\pm 2/\pm 0,-1)$			A2
414A	R-22/124/600a/142b (51.0/28.5/4.0/16.5)	$(\pm 2/\pm 2/\pm 0.5/\pm 0.5, -1)$			A1
414B	R-22/124/600a/142b (50.0/39.0/1.5/9.5)	$(\pm 2/\pm 2/\pm 0.5/\pm 0.5,-1)$			A1
415A	R-22/152a (82.0/18.0)	(±1/±1)			A2
415B	R-22/152a (25.0/75.0)	(±1/±1)			A2
416A	R-134a/124/600 (59.0/39.5/1.5)	(+0.5,-1/+1,-0.5/+1,-0.2)			A1
417A	R-125/134a/600 (46.6/50.0/3.4)	$(\pm 1/\pm 1/\pm 0.1, -0.4)$			A1
418A	R-290/22/152a (1.5/96.0/2.5)	$(\pm 0.5/\pm 1/\pm 0.5)$			A2
419A	R-125/134a/E170 (77.0/19.0/4.0)	$(\pm 1/\pm 1/\pm 1)$			A2
420A	R-134a/142b (88.0/12.0)	$(\pm 1, -0, \pm 0, -1)$			A1
421A	R-125/134a (58.0/42.0)	$(\pm 1/\pm 1)$			A1
421B	R125/134a (85.0/15.0)	(±1/±1)			A1
422A	R-125/134a/600a (85.1/11.5/3.4)	$(\pm 1/\pm 1/+0.1,-0.4)$			A1
422B	R-125/134a/600a (55.0/42.0/3.0)	$(\pm 1/\pm 1/+0.1,-0.5)$			A1
422C	R-125/134a/600a (82.0/15.0/3.0)	$(\pm 1/\pm 1/+0.1,-0.5)$			A1
	R-134a/227ea (52.5/47.5)	$(\pm 1/\pm 1)$			A1
424A	R-125/134a/600a/600/601a (50.5/47.0/0.9/1.0/0.6)	$(\pm 1/\pm 1/+0.1,-0.2/+0.1, -0.2/+0.1,-0.2)$			A1
425A	R-32/134a/227ea (18.5/69.5/12.0)	$(\pm 0.5/\pm 0.5/\pm 0.5)$			A1
425A 426A	R-125/134a/600a/601a (5.1/93.0/1.3/0.6)	$(\pm 0.3/\pm 0.3/\pm 0.3)$ $(\pm 1/\pm 1/+0.1,-0.2/+0.1,-0.2)$			A1
	R-32/125/143a/134a (15.0/25.0/10.0/50.0)	$(\pm 1/\pm 1/\pm 0.1, -0.2/\pm 0.1, -0.2)$ $(\pm 2/\pm 2/\pm 2/\pm 2)$			A1
	R-125/143a/290/600a (77.5/20.0/0.6/1.9)	$(\pm 1/\pm 1/+0.1, -0.2/+0.1, -0.2)$			A1
Azeotropesb		(-, -, -, -, -, -, -, -, -, -, -, -, -,			
500	R-12/152a (73.8/26.2)		0	99.3 –33	A1
	R-22/12 (75.0/25.0) ^c		-4 1	93.1 –41	A1
502	R-22/115 (48.8/51.2)		19	112.0 –45	A1
503	R-23/13 (40.1/59.9)		88	87.5 -88	
504	R-32/115 (48.2/51.8)		17	79.2 –57	
	R-12/31 (78.0/22.0) ^c		115	103.5 –30	
	R-31/114 (55.1/44.9)		18	93.7 –12	
	R-125/143a (50.0/50.0)		-4 0	98.9 –46.7	A1
508A ^d	R-23/116 (39.0/61.0)		-86	100.1 -86	A1
	R-23/116 (46.0/54.0)		-45.6	95.4 -88.3	A1

Source: ANSI/ASHRAE Standard 34-2007.

^aMolecular mass and normal boiling point are not part of this standard.

^bAzeotropic refrigerants exhibit some segregation of components at conditions of temperature and pressure other than those at which they were formulated. Extent of segregation depends on the particular azeotrope and hardware system configuration.

^cExact composition of this azeotrope is in question, and additional experimental studies are

needed. $^{\rm d}$ R-507, R-508, and R-509 are allowed designations for R-507A, R-508A, and R-509A because of a change in designations after assignment of R-500 through R-509. Corresponding changes were not made for R-500 through R-506.

Global Environmental Characteristics of Refrigerants. Atmospheric release of CFC and HCFC refrigerants such as R-11, R-12, R-22, and R-502 contributes to depletion of the ozone layer. The measure of a material's ability to deplete stratospheric ozone is its **ozone depletion potential (ODP)**, a value relative to that of R-11 which is 1.0.

Halocarbons (CFCs, HCFCs, and HFCs) and many nonhalocarbons (e.g., hydrocarbons, carbon dioxide) are also greenhouse gases. The **global warming potential (GWP)** of a GHG is an index describing its relative ability to trap radiant energy compared to $\rm CO_2$ (R-744), which has a very long atmospheric lifetime. GWP may be calculated for any particular **integration time horizon (ITH)**. Typically, a 100 year ITH is used for regulatory purposes, and may be designated as $\rm GWP_{100}$.

The energy refrigeration appliances consume is often produced from fossil fuels, which results in emission of CO_2 , a contributor to global warming. This indirect effect associated with energy consumption is frequently much larger than the direct effect of refrigerant emissions. The **total equivalent warming impact (TEWI)** of an HVAC&R system is the sum of direct refrigerant emissions expressed in terms of CO_2 equivalents, and indirect emissions of CO_2 from the system's energy use over its service life. Another measure is **life-cycle climate performance (LCCP)**, which includes TEWI and adds direct and indirect emissions effects associated with manufacturing the refrigerant.

Ammonia (R-717), hydrocarbons, HCFCs, and most HFCs have shorter atmospheric lifetimes than CFCs because they are largely destroyed in the lower atmosphere by reactions with OH radicals. A shorter atmospheric lifetime generally results in lower ODP and GWP₁₀₀ values. Environmentally preferred refrigerants (1) have

Table 3 Refrigerant Environmental Properties

Refrigerant	Atmospheric Lifetime, years ^a	ODP ^b	GWP ₁₀₀ ^c
R-11	45	1	4750
R-12	100	1	10 900
R-13	640	1	14 400
R-22	12	0.055	1810
R-23	270	0	14 800
R-32	4.9	0	675
R-113	85	0.8	6130
R-114	300	1	10 000
R-115	1700	0.6	7370
R-116	10 000	0	12 200
R-123	1.3	0.02	77
R-124	5.8	0.022	609
R-125	29	0	3500
R-134a	14	0	1430
R-141b	9.3	0.11	725
R-142b	17.9	0.065	2310
R-143a	52	0	4470
R-152a	1.4	0	124
R-218	2600	0	8830
R-227ea	34.2	0	3220
R-236fa	240	0	9810
R-245ca	6.2 ^d	0	693 ^d
R-245fa	7.6	0	1030
R-C318	3200	0	10 300
R-744	Variable	0	1
R-290	0.41 ^d	0	~20 ^d
R-600	0.018 ^d	0	~20 ^d
R-600a	0.019 ^d	0	~20 ^d
R-601a	0.01 ^d	0	~20 ^d
R-717	0.01 ^d	0	<1 ^d
R-1270	0.001 ^d	0	~20 ^d

^aAtmospheric lifetimes from Table 2.14 of IPCC (2007b) except where indicated. ^bODP from UNEP (2006), Section 1.1, Annexes A, B, and C, pp. 23-25.

low or zero ODP, (2) have relatively short atmospheric lifetimes, (3) have low GWP_{100} , (4) provide good system efficiency, (5) have appropriate safety properties, and (6) yield a low TEWI or LCCP in system applications (i.e., leaks are minimized or prevented, and performance is optimized).

Table 3 shows atmospheric lifetime, ODP, and GWP_{100} of refrigerants being phased out under the Montreal Protocol and of refrigerants being used to replace them, alone or as components of blends. Because HFCs do not contain chlorine or bromine, their ODP values are negligible (Ravishankara et al. 1994) and thus are shown as 0 in Table 3. Nonhalocarbon refrigerants listed have zero ODP and very low GWP_{100} .

There are some differences between the values stipulated for reporting under the Montreal and Kyoto protocols and the latest scientific values. These are not of sufficient magnitude to significantly alter design decisions based on the numbers in the table. All these values have rather wide error bands and may change with each assessment of the science. Changes in GWP assessments are largely dominated by changes in understanding of CO₂, which is the reference chemical.

Table 4 shows the calculated ODPs and GWP_{100} s for refrigerant blends, using the latest scientific assessment values as reported in Calm and Hourahan (2007).

Physical Properties

Table 5 lists some physical properties of commonly used refrigerants, a few very-low-boiling-point cryogenic fluids, some newer refrigerants, and some older refrigerants of historical interest. These refrigerants are arranged in increasing order of atmospheric boiling point.

Table 5 also includes the freezing point, critical properties, and refractive index. Of these properties, normal boiling point is most important because it is a direct indicator of the temperature at which a refrigerant can be used. The freezing point must be lower than any contemplated usage. The critical properties describe a material at the

Table 4 Environmental Properties of Refrigerant Blends

Refrigera	nt		Refrigera	nt	
Number	ODP*	$GWP_{100}*$	Number	ODP*	$GWP_{100}*$
401A	0.033	1200	415B	0.013	550
401B	0.036	1300	416A	0.008	1100
401C	0.027	930	417A	0.000	2300
402A	0.019	2800	418A	0.048	1700
402B	0.030	2400	419A	0	3000
403A	0.038	3100	420A	0.008	1500
403B	0.028	4500	421A	0	2600
404A	0	3900	421B	0	3200
405A	0.026	5300	422A	0	3100
406A	0.056	1900	422B	0	2500
407A	0	2100	422C	0	3100
407B	0	2800	422D	0	2700
407C	0	1800	423A	0	2300
407D	0	1600	424A	0	2400
407E	0	1600	425A	0	1500
408A	0.024	3200	426A	0	1500
409A	0.046	1600	427A	0	2100
409B	0.045	1600	428A	0	3600
410A	0	2100	500	0.738	8100
411A	0.044	1600	502	0.250	4700
411B	0.047	1700	503	0.599	15 000
412A	0.053	2300	507A	0	4000
413A	0	2100	508A	0	13 000
414A	0.043	1500	508B	0	13 000
414B	0.039	1400	509A	0.022	5700
415A	0.028	1500			

^{*}ODPs and GWP_{100} s from Calm and Hourahan (2007), computed based on mass-weighted averages of values for individual components.

^cGWP₁₀₀ from Table 2.14 of IPCC (2007b) except where indicated.

dCalm and Hourahan (2007).

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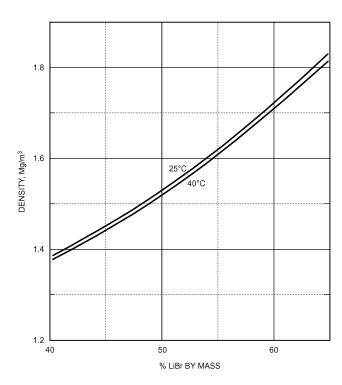


Fig. 1 Specific Density of Aqueous Solutions of Lithium Bromide

point where the distinction between liquid and gas is lost. At higher temperatures, no separate liquid phase is possible for pure fluids. In refrigeration cycles involving condensation, a refrigerant must be chosen that allows this change of state to occur at a temperature somewhat below the critical. Cycles that reject heat at supercritical temperatures (such as cycles using carbon dioxide) are also possible.

Lithium Bromide/Water and Ammonia/Water Solutions. These are the most commonly used working fluids in absorption refrigeration systems. Figure 1 shows density, Figure 2 shows specific heat, and Figure 3 shows viscosity of lithium bromide/water solutions. Chapter 30 has an enthalpy-concentration diagram and a vapor pressure diagram for lithium bromide/water solutions. Chapter 30 also has equilibrium properties of water/ammonia solutions.

Electrical Properties

Tables 6 and 7 list the electrical characteristics of refrigerants that are especially important in hermetic systems.

Sound Velocity

The practical velocity of a gas in piping or through openings is limited by the velocity of sound in the gas.

Table 8 gives examples of the velocity of sound in the vapor phase of various refrigerants. Chapter 30 has sound velocity data for many refrigerants. The velocity increases when temperature is increased and decreases when pressure is increased. The velocity of sound can be calculated from the equation

$$V_a = \sqrt{(dp/d\rho)_S} = \sqrt{\gamma (dp/d\rho)_T}$$
 (1)

where

 V_a = sound velocity, m/s

p = pressure, Pa

 $\rho = \text{density}, \text{kg/m}^3$

 $\gamma = c_p/c_v = \text{ratio of specific heats}$

 $S = \text{entropy}, \text{kJ/(kg} \cdot \text{K)}$

T =temperature, K

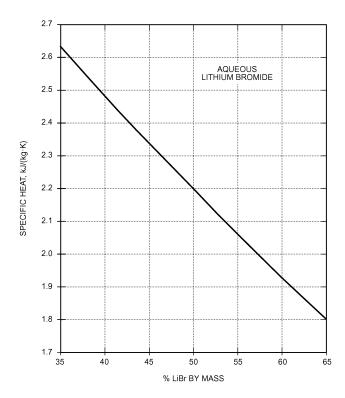


Fig. 2 Specific Heat of Aqueous Lithium Bromide Solutions

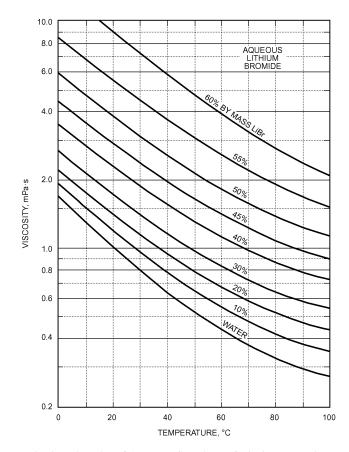


Fig. 3 Viscosity of Aqueous Solutions of Lithium Bromide

Table 5 Physical Properties of Selected Refrigerants^a

-	Refrigerant			Dailing Dt	Eucoging	Critical	Cuitical	Critical	Defuestive
No.	Chemical Name or Composition (% by Mass)	Chemical Formula	Molecular Mass	Boiling Pt. (NBP) at 101.325 kPa, °C	Freezing Point, °C	Temperature, °C	Critical Pressure, kPa	Density, kg/m ³	Refractive Index of Liquid ^{b,c}
728	Nitrogen	N_2	28.013	-195.8	-210.0	-146.96	3395.8	313.3	1.205 (83 K) 589.3 nm
729	Air	_	28.959	-194.25	_	-140.59	3789.6	335.94	_
740	Argon	Ar	39.948	-185.85	-189.34	-122.46	4863.0	535.6	1.233 (84 K) 589.3 nm
732	Oxygen	O_2	31.999	-182.96	-218.79	-118.57	5043.0	436.14	1.221 (92 K) 589.3 nm
50	Methane	CH_4	16.043	-161.48	-182.46	-82.586	4599.2	162.66	_
14	Tetrafluoromethane	CF_4	88.005	-128.05	-183.61	-45.64	3750.0	625.66	_
170	Ethane	C_2H_6	30.07	-88.581	-182.8	32.72	4872.2	206.18	_
503	R-23/13 (40.1/59.9)	_	87.247	-87.76	_	18.417	4280.5	565.68	_
$508A^{4}$	R-23/116 (39/61)	_	100.1	-87.233	_	10.192	3650.8	567.58	_
$508B^4$	R-23/116 (46/54)	_	95.394	-87.206	_	11.205	3771.6	568.45	_
23	Trifluoromethane	CHF_3	70.014	-82.018	-155.13	26.143	4832	526.5	_
13	Chlorotrifluoromethane	CClF ₃	104.46	-81.48	-181.15	28.85	3879	582.88	$1.146(25)^2$
744	Carbon dioxide	CO_2	44.01	-78.4^{d}	-56.558e	30.978	7377.3	467.6	1.195 (15)
504	R-32/115 (48.2/51.8)	_	79.249	-57.906	_	62.138	4428.8	504.68	_ ` `
32	Difluoromethane	CH_2F_2	52.024	-51.651	-136.81	78.105	5782.0	424	_
410A	R-32/125 (50/50)		72.585	-51.446	_	71.358	4902.6	459.53	_
125	Pentafluoroethane	C ₂ HF ₅	120.02	-48.09	-100.63	66.023	3617.7	573.58	_
1270	Propylene	C_3H_6	42.08	-47.62	-185.2	91.061	4554.8	230.03	$1.3640 (-50)^{1}$
143a	Trifluoroethane	CH ₃ CF ₃	84.041	-47.241	-111.81	72.707	3761.0	431.0	_ ` ´
507A	R-125/143a (50/50)	_	98.859	-46.741	_	70.617	3705	490.77	_
	R-125/143a/134a (44/52/4)	_	97.604	-46.222	_	72.046	3728.9	486.53	_
502	R-22/115 (48.8/51.2)	_	111.63	-45.174	_	80.507	4016.8	568.70	_
407C	R-32/125/134a (23/25/52)	_	86.204	-43.627	_	86.034	4629.8	484.23	_
290	Propane	C_3H_8	44.096	-42.11	-187.62	96.74	4251.2	220.4	1.3397 (-42)
22	Chlorodifluoromethane	CHClF ₂	86.468	-40.81	-157.42	96.145	4990.0	523.84	$1.234(25)^2$
115	Chloropentafluoroethane	CCIF ₂ CF ₃	154.47	-39.25	-99.39	79.95	3129.0	614.8	$1.221 (25)^2$
500	R-12/152a (73.8/26.2)		99.303	-33.603	_	102.09	4168.6	495.1	_ ` `
717	Ammonia	NH_3	17.03	-33.327	-77.655	132.25	11 333.0	225.0 ^d	1.325 (16.5)
12	Dichlorodifluoromethane	CCl ₂ F ₂	120.91	-29.752	-157.05	111.97	4136.1	565.0	$1.288(25)^{2}$
134a	Tetrafluoroethane	CF ₃ CH ₂ F	102.03	-26.074	-103.3	101.06	4059.3	511.9	_ ` `
152a	Difluoroethane	CHF ₂ CH ₃	66.051	-24.023	-118.59	113.26	4516.8	368	_
124	Chlorotetrafluoroethane	CHClFCF ₃		-11.963	-199.15	122.28	3624.3	560.0	_
600a	Isobutane	C_4H_{10}	58.122	-11.75	-159.42	134.66	3629.0	225.5	1.3514 (-25) ¹
142b	Chlorodifluoroethane	CClF ₂ CH ₃	100.5	-9.15	-130.43	137.11	4055.0	466.0	_
C318	Octafluorocyclobutane	C_4F_8	200.03	-5.975	-39.8	115.23	2777.5	619.97	
600	Butane	C_4H_{10}	58.122	-0.49	-102.7	151.98	3796.0	227.94	1.3562 (-15) ¹
114	Dichlorotetrafluoroethane	CClF ₂ CClF ₂		3.586	-94.15	145.68	3257.0	579.97	1.294 (25)
11	Trichlorofluoromethane	CCl ₃ F	137.37	23.708	-110.47	197.96	4407.6	554.0	$1.362 (25)^2$
123	Dichlorotrifluoroethane	CHCl ₂ CF ₃	152.93	27.823	-107.15	183.68	3661.8	550.0	_
141b	Dichlorofluoroethane	CCl ₂ FCH ₃	116.95	32.05	-103.5	204.4	4212.0	458.6	_
113	Trichlorotrifluoroethane	CCl ₂ FCClF ₂		47.585	-36.22	214.06	3392.2	560.0	$1.357(25)^2$
718^{3}	Water	H ₂ O	18.015	99.974	0.01	373.95	22 064.0	322.0	_

Notes:

Sound velocity can be estimated from tables of thermodynamic properties. Change in pressure with a change in density $(dp/d\rho)$ can be estimated at either constant entropy or constant temperature. It is simpler to estimate at constant temperature, but the ratio of specific heats must also be known.

REFRIGERANT PERFORMANCE

Chapter 2 describes several methods of calculating refrigerant performance, and Chapter 30 includes tables of thermodynamic properties of refrigerants.

Table 9 shows the theoretical calculated performance of a number of refrigerants for a standard cycle of 258 K evaporation and 303 K condensation. In most cases, suction vapor is assumed to be saturated, and compression is assumed adiabatic or at constant entropy. For R-113 and R-114, for example, these assumptions cause some liquid in the discharge vapor. In these cases, it is assumed that discharge vapor is saturated and that suction vapor is slightly superheated. Note that actual operating conditions and performance differ somewhat from numbers in the table because of additional factors such as compressor efficiency and transport properties.

^aData from NIST (2007) REFPROP v. 8.0.

^bTemperature of measurement (°C, unless kelvin is noted) shown in parentheses. Data from CRC (1987), unless otherwise noted.

cFor the sodium D line.

^dSublimes.

eAt 527 kPa.

References:

¹Kirk and Othmer (1956).

²Bulletin B-32A (DuPont). ³Handbook of Chemistry (1967).

⁴NIST Standard Reference Database 23, v. 7 (Lemmon et al. 2002).

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Table 6 Electrical Properties of Liquid Refrigerants

Refrigerant			•		
				Volume	
No	Chemical Name or	Temp., °C	Dielectric	Resistivity MΩ·m	*
No.	Composition (% By Mass)		Constant	MC2·m	Ref.
11	Trichlorofluoromethane	28.9	2.28		1
		a	1.92	63 680	2
		25	2.5	90	3
		25	2.32		10
12	Dichlorodifluoromethane	28.9	2.13		1
		a	1.74	53 900	2
		25	2.1	>120	3
		25	2.100		4
		25	2.14		10
13	Chlorotrifluoromethane	-30	2.3	120	4
		20	1.64		
22	Chlorodifluoromethane	23.9	6.11		1
		a	6.12	0.83	2
		25	6.6	75	3
		25	6.42		10
23	Trifluoromethane	-30	6.3		3
		20	5.51		4
32	Difluoromethane	a	14.27		6
		25	14.67		10
113	Trichlorotrifluoroethane	30	2.44		1
110		a	1.68	45 490	2
		25	2.6	>120	3
114	Dichlorotetrafluoroethane	31.1	2.17	- 120	1
117	Biemorotetrariuoroetriane	a a	1.83	66 470	2
		25	2.2	>70	3
123	2,2-dichloro-1,1,1-		4.50	14 700	7
123	trifluoroethane	a	4.50	14 /00	,
124	2-chloro-1,1,1,2-	25	4.89		10
	tetrafluoroethane		,		
124a	Chlorotetrafluoroethane	25	4.0	50	3
125	Pentafluoroethane	20	4.94		8
		25	5.10		10
134a	1,1,1,2-tetrafluoroethane	a	9.51	17 700	7
	, , ,	25	9.87		10
143a	1,1,1-trifluoroethane	25	9.78		10
236fa		25	7.89		10
245fa	1,1,1,3,3-pentafluoropropane	25	6.82		10
290	Propane	a	1.27	73 840	2
	R-125/143a/134a (44/52/4)	a	7.58	8450	9
	16 120/1 10 10 10 (1 1/02/1)	25	8.06	0.50	10
407C	R-32/125/134a (23/25/52)	a	8.74	7420	9
4070	1C-32/123/13-4a (23/23/32)	25	10.21	7420	10
4104	R-32/125 (50/50)	a	7.78	3920	9
410A	K-32/123 (30/30)	25		3920	
500	D 12/152a (72.9/26.2)		5.37	55 750	10
500	R-12/152a (73.8/26.2)	a	1.80	55 750	2
507A	R-125/143a (50/50)	a 25	6.97	5570	9
500 4	D 22/116 (20/61)	25	7.94		10
308A	R-23/116 (39/61)	-30	6.60		1
5005	D 00/11/6 (4/6/5/1)	0	5.02		1
508B	R-23/116 (46/54)	-30	7.24		1
=1-		0	5.48		1
717	Ammonia	20.6	15.5		5
744	Carbon dioxide	0	1.59		5
	bient temperature		5 CRC (198		
Referer	nces: from E.I. DuPont de Nemours & Co	Inc	6 Bararo et a 7 Fellows et		
	ham and Divers (1955)	.,	8 Pereira et		
3 Eiser	man (1955)		9 Meurer et	al. (2001)	
4 Fello	ws et al. (1991)		10 Gbur (200	(5)	

Table 7 Electrical Properties of Refrigerant Vapors

No.	Refrigerant Chemical Name or Composition (% by mass)	Pres- sure, kPa	Temp., °C		Relative Dielectric Strength, Nitrogen = 1	Volume Resis- tivity, GΩ·m	Ref
11	Trichlorofluoro-	50.7	26.1	1.0019			3
	methane	a	b	1.009		74.35	2
		101.3	22.8		3.1		4
12	Dichlorodifluoro- methane	50.7	28.9	1.0016			3
	memane	a	b	1.012	452°	72.77	2
		101.3	22.8		2.4		4
1.2	C11	101.3	25	1.0064			6
13	Chlorotrifluoro- methane	50.7	28.9	1.0013	1.4		3
14	Tetrafluoromethane	101.3 50.7	22.8	1.0006	1.4		3
14	retratituorottiettiane	101.3	22.8	1.0000	1.0		4
22	Chlorodifluoro-	50.7	22.0	1.0035	1.0		3
22	methane	a	b	1.0033	460°	2113	2
		101.3	22.8	1.001	1.3	2113	4
		101.3	25	1.0068	1.5		6
32	Difluoromethane	101.3	25	1.0102			6
113	Trichlorotri-	a	b	1.010	440°	94.18	2
	fluoroethane	40.5	22.8		2.6		4
114	Dichlorotetra-	50.7	26.7	1.0021			3
	fluoroethane	a	b	1.002	295°	148.3	2
		101.3	22.8		2.8		4
116	Hexafluoroethane	95.2	22.8	1.002			3
124	2-chloro-1,1,1,2- tetrafluoroethane	101.3	25	1.0060			6
125	Pentafluoroethane	101.3	25	1.0072			6
134a	1,1,1,2-	101.3	25	1.0125			6
	tetrafluoroethane						
142b	Chlorodifluoroethane	94.2	27.2	1.013			3
143a	Trifluoroethane	86.1	25	1.013			3
		101.3	25	1.0170			6
170	Ethane	101.3	0	1.0015			1
236fa	1,1,1,3,3,3- hexafluoropropane	101.3	25	1.0121			6
245fa	1,1,1,3,3-	101.3	25	1.0066			6
200	pentafluoropropane		1.	1.000	4.400	105.2	
290 404 A	Propane R-125/143a/134a	a 101.3	b	1.009	440°	105.3	2
404A	(44/52/4)	101.3	25	1.0121			6
407C	R-32/125/134a (23/25/52)	101.3	25	1.0113			6
410A	R-32/125 (50/50)	101.3	25	1.0078			6
500	R-12/152a (73.8/26.2)	a	b	1.024	470°	76.45	2
507A	R-125/143a (50/50)	101.3	25	1.0119			6
508A	R-23/116 (39/61)	a	-30	1.12			5
		a	0	1.31			5
		101.3	25	1.0042			6
508B	R-23/116 (46/54)	a	-30	1.13			5
		a	0	1.34			5
		101.3	25	1.0042			6
717	Ammonia	101.3	0	1.0072	0.65		1
, . ,		a	0	1.000=	0.82		4
			0	1.00059	1		1
729	Air	101.3			1		-
729	Air Carbon dioxide	101.3	0	1.00099			1
729 744					0.88		1 4

⁴ Fellows et al. (1991)

¹⁰ Gbur (2005)

a = saturation vapor pressure
b = ambient temperature
c = measured breakdown voltage, volts/mil
References:
1 CRC (1987)

³ Fuoss (1938)
4 Charlton and Cooper (1937)
5 Data from E.I. DuPont de Nemours &

Co., Inc. 6 Gbur (2005)

Table 8 Velocity of Sound in Refrigerant Vapors

Tabl	e o velocit	· • •							
	_	Temperature, °C							
	Pressure, _	10	50	100					
Refrigerant	kPa	Ve	locity of Sound,	m/s					
11	100	b	144.52	156.06					
12	100	145.94	156.20	167.93					
	1000	b	136.60	156.04					
22	1500	b	b	148.45					
22	100 1000	177.08 b	188.81 173.97	202.24 193.09					
	1500	b	163.78	187.56					
23	100	199.83	212.33	226.78					
23	1000	188.21	204.92	222.29					
	1500	180.89	200.66	219.83					
32	100	235.50	250.33	267.05					
	1000	212.11	236.68	258.78					
	1500	b	228.18	254.02					
113	100	b	119.64	130.01					
114	100	118.04	127.18	137.39					
123	100	b	134.30	145.46					
	1000	b	b	b					
10.4	1500	b	b	155.12					
124	100 1000	133.96	143.96	155.12 139.55					
	1500	b b	b b	139.33					
134a	100	157.21	168.39	180.99					
1374	1000	b	146.88	168.59					
	1500	b	b	160.87					
143a	100	174.73	186.74	200.45					
	1000	b	168.36	189.26					
	1500	b	156.00	182.68					
404A	100	161.39	172.60	185.37					
	1000	b	155.51	178.05					
	1500	b	143.93	168.98					
407C	100	173.85	185.72	199.20					
	1000	b	169.30	189.38					
410A	1500	b 192.84	158.12 205.56	183.56 220.06					
410A	1000	170.15	192.17	211.92					
	1500	b	183.78	207.24					
502	100	152.01	162.45	174.43					
	1000	b	147.40	165.17					
	1500	b	136.70	159.59					
507A	100	160.32	174.45	184.14					
	1000	b	154.67	174.00					
	1500	b	143.34	168.04					
508A	100	161.68	172.35	184.74					
	1000 1500	149.98 142.71	164.89 160.67	180.22 177.84					
508B	100	166.23	177.14	189.76					
300D	1000	154.64	169.74	185.31					
	1500	147.46	165.55	182.94					
600	100	204.59	219.88	236.83					
	1000	b	b	206.17					
	1500	b	b	181.53					
600a	100	205.58	220.45	237.15					
	1000	b	b	210.17					
	1500	b	b	190.26					
717	100	422.02	450.44	482.17					
	1000	b	430.71	470.71					
711	1500	b	417.84	463.93					
744	100 1000	262.37 253.98	278.69 273.23	297.64 294.31					
	1500	233.98	273.23	294.31					
	1500	4-10./J	2/0.12	2,2.40					

Source: NIST Standard Reference Database 23, v.7.0 (Lemmon et al. 2002)

b = Below saturation temperature.

SAFETY

Tables 1 and 2 summarize toxicity and flammability characteristics of many refrigerants. In ASHRAE *Standard* 34, refrigerants are classified according to the hazard involved in their use. The toxicity and flammability classifications yield six safety groups (A1, A2, A3, B1, B2, and B3) for refrigerants. Group A1 refrigerants are the least hazardous, Group B3 the most hazardous.

The safety classification in ASHRAE *Standard* 34 consists of a capital letter and a numeral. The capital letter designates a toxicity class based on allowable exposure:

- Class A: Toxicity has not been identified at concentrations less than or equal to 400 ppm by volume, based on data used to determine threshold limit value/time-weighted average (TLV/TWA) or consistent indices.
- Class B: There is evidence of toxicity at concentrations below 400 ppm by volume, based on data used to determine TLV/TWA or consistent indices.

The numeral denotes flammability:

- Class 1: No flame propagation in air at 21°C and 101 kPa
- Class 2: Lower flammability limit (LFL) greater than 0.10 kg/m³ at 21°C and 101 kPa and heat of combustion less than 19 000 kJ/kg
- Class 3: Highly flammable as defined by LFL less than or equal to 0.10 kg/m³ at 21°C and 101 kPa or heat of combustion greater than or equal to 19 000 kJ/kg

LEAK DETECTION

Leak detection in refrigeration equipment is of major importance for manufacturers and service engineers.

Electronic Detection

Electronic detectors are widely used in manufacture and assembly of refrigeration equipment. Instrument operation depends on the variation in current flow caused by ionization of decomposed refrigerant between two oppositely charged platinum electrodes. This instrument can detect any of the halogenated refrigerants except R-14; however, it is not recommended for use in atmospheres that contain explosive or flammable vapors. Other vapors, such as alcohol and carbon monoxide, may interfere with the test.

The electronic detector is the most sensitive of the various leak detection methods, reportedly capable of sensing a leak of 0.3 g of R-12 per year. A portable model is available for field testing. Other models are available with automatic balancing systems that correct for refrigerant vapors that might be present in the atmosphere around the test area.

Bubble Method

The object to be tested is pressurized with air or nitrogen. A pressure corresponding to operating conditions is generally used. If possible, the object is immersed in water, and any leaks are detected by observing bubbles in the liquid. Adding a detergent to the water decreases surface tension, prevents escaping gas from clinging to the side of the object, and promotes formation of a regular stream of small bubbles. Kerosene or other organic liquids are sometimes used for the same reason. A solution of soap or detergent can be brushed or poured onto joints or other spots where leakage is suspected. Leaking gas forms soap bubbles that can be readily detected.

Leaks can also be determined by pressurizing or evacuating and observing the change in pressure or vacuum over a period of time. This is effective in checking system tightness but does not locate the point of leakage.

UV Dye Method

A stable UV-fluorescent dye is introduced into the system to be tested. Operating the system mixes the UV dye uniformly in the

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Table 9 Comparative Refrigerant Performance per Ton of Refrigeration

	Refrigerant							Specific				Com-
No.	Chemical Name or Composition (% by mass)	Evap- orator Pressure, MPa	Con- denser Pressure, MPa	Com- pression Ratio	Net Refrig- erating Effect, kJ/kg	Refrig- erant Circu- lated, g/s	Liquid Circu- lated, L/s	Volume of Suction Gas, m ³ /kg	Com- pressor Displace- ment, L/s	Power Consump- tion, kW	Coeffi- cient of Perform- ance	pressor Discharge Temp., °C
170	Ethane	1.608	4.639	2.88	161.71	6.10	0.0219	0.0338	0.206	0.365	2.7	323
744	Carbon dioxide	2.254	7.18	3.19	133.23	3.88	0.0064	0.0168	0.065	0.192	2.69	343
1270	Propylene	0.358	1.304	3.64	286.17	3.46	0.0070	0.1299	0.449	0.220	4.5	315
290	Propane	0.286	1.075	3.76	277.90	3.53	0.0073	0.1562	0.551	0.218	4.5	309
502	R-22/115 (48.8/51.2)	0.343	1.312	3.83	105.95	9.43	0.0079	0.0508	0.479	0.228	4.38	311
507A	R-125/143a (50/50)	0.379	1.459	3.85	110.14	9.07	0.0089	0.0508	0.461	0.239	4.18	308
404A	R-125/143a/134a (44/52/4)	0.365	1.42	3.89	114.15	8.75	0.0086	0.0537	0.470	0.237	4.21	309
410A	R-32/125 (50/50)	0.478	1.872	3.92	167.89	5.84	0.0056	0.0545	0.318	0.222	4.41	324
125	Pentafluoroethane	0.403	1.561	3.87	85.30	11.41	0.0098	0.0394	0.449	0.244	3.99	304
22	Chlorodifluoromethane	0.295	1.187	4.02	162.67	6.13	0.0052	0.0779	0.478	0.214	4.66	326
12	Dichlorodifluoromethane	0.181	0.741	4.09	117.02	8.49	0.0066	0.0923	0.784	0.212	4.7	311
500	R-12/152a (73.8/26.2)	0.214	0.876	4.09	139.68	7.08	0.0063	0.0939	0.665	0.212	4.66	314
407C	R-32/125/134a (23/25/52)	0.288	1.26	4.38	163.27	6.11	0.0054	0.0805	0.492	0.222	4.5	321
600a	Isobutane*	0.088	0.403	4.58	263.91	3.76	0.0069	0.4073	1.533	0.215	4.62	303
134a	Tetrafluoroethane	0.163	0.767	4.71	148.03	6.71	0.0056	50.1214	0.814	0.216	4.6	310
124	Chlorotetrafluoroethane*	0.0088	0.443	5.03	117.83	8.41	0.0063	0.1711	11.439	0.214	4.62	303
717	Ammonia	0.235	1.162	4.94	1103.1	0.90	0.0015	0.5117	0.463	0.210	4.76	372
600	Butane*	0.056	0.283	5.05	292.24	3.53	0.0062	0.6446	2.274	0.218	4.74	303
11	Trichlorofluoromethane	0.02	0.125	6.25	155.95	6.36	0.0043	0.7689	4.891	0.197	5.02	316
123	Dichlorotrifluoroethane	0.016	0.109	6.81	142.28	7.02	0.0048	0.8914	6.259	0.204	4.9	306
113	Trichlorotrifluoroethane*	0.007	0.054	7.71	122.58	7.84	0.0051	1.6818	13.187	0.200	4.81	303

^{*}Superheat required.

oil/refrigerant system. The dye, which usually prefers oil, shows up at the leak's location, and can be detected using an appropriate UV lamp. Ensure that the dye is compatible with system components and that no one is exposed to UV radiation from the lamp. This method is often more effective for liquid leaks than for vapor.

Another, more expensive method is to use dispersive and nondispersive infrared analyzers. Although these analyzers are expensive, they can not only find the refrigerant leak but also identify the refrigerant.

Ammonia Leaks

Ammonia can be detected by any of the previously described methods, or by bringing a solution of hydrochloric acid near the object. If ammonia vapor is present, a white cloud or smoke of ammonium chloride forms. Ammonia can also be detected with indicator paper that changes color in the presence of a base.

EFFECT ON CONSTRUCTION MATERIALS

Metals

Halogenated refrigerants can be used satisfactorily under normal conditions with most common metals, such as steel, cast iron, brass, copper, tin, lead, and aluminum. Under more severe conditions, various metals affect properties such as hydrolysis and thermal decomposition in varying degrees. The tendency of metals to promote thermal decomposition of halogenated compounds is in the following order:

(least decomposition) Inconel < 18-8 stainless steel < nickel < copper < 1040 steel < aluminum < bronze < brass < zinc < silver (most decomposition)

This order is only approximate, and there may be exceptions for individual compounds or for special use conditions. The effect of metals on hydrolysis is probably similar.

Table 10 Swelling of Elastomers in Liquid Refrigerants at Room Temperature, % Linear Swell

Refrig- erant Number	Polyiso- prene (Sulfur Cure)	Poly- chloro- prene	Butyl Rubber	Styrene Buta- diene Rubber	Nitrile Rubber	Fluoro- elastomer
22	10.2	6.1	3.9	9.8	51.4	33.2
123	48.0	15.3	16.3	40.8	83.7	31.6
124	5.8	2.8	3.2	4.1	45.9	29.0
142b	10.2	6.5	6.2	7.3	8.7	31.8
32	2.7	1.0	1.0	2.0	8.3	23.2
125	4.2	2.7	2.6	3.6	3.9	11.7
134a	1.2	1.2	0.6	1.0	5.1	25.6
143a	1.9	1.2	1.3	1.5	2.0	13.6
152a	4.2	3.0	1.7	2.8	8.8	3.91

Magnesium alloys and aluminum containing more than 2% magnesium are not recommended for use with halogenated compounds where even trace amounts of water may be present. Zinc is not recommended for use with CFC-113. Experience with zinc and other fluorinated compounds has been limited, but no unusual reactivity has been observed under normal conditions of use in dry systems.

Ammonia should never be used with copper, brass, or other alloys containing copper. Further discussion of the compatibility of refrigerants and lubricants with construction materials may be found in Chapter 5 of the 2006 ASHRAE Handbook—Refrigeration.

Elastomers

Linear swelling of some elastomers in the liquid phase of HCFC and HFC refrigerants is shown in Table 10. Swelling data can be used to a limited extent in comparing the effect of refrigerants on elastomers. However, other factors, such as the amount of extraction, tensile strength, and degree of hardness of the exposed elastomer, must be considered. When other fluids (e.g., lubricants) are present in addition to the refrigerant, the combined effect on elastomers should be determined. Extensive test data for compatibility of elastomers and gasketing materials with refrigerants and lubricants

Table 11 Diffusion of Water and R-22 Through Elastomers

	Diffusion Rate			
Elastomer	Water ^a	R-22b		
Polychloroprene	970	4.63		
Nitrile rubber	150	69.4		
Chlorosulfonated polyethylene	620	1.85		
Butyl rubber	58	1.04		
Fluoroelastomer	_	12.7		
Polyethylene	167	_		
Natural	1940	_		

Adapted from Eiseman (1955).

are reported by Hammed et al. (1994). Diffusion of fluids through elastomers is another consideration; Table 11 shows the diffusion rate of water and R-22 through elastomers.

Plastics

The effect of a refrigerant on a plastic material should be thoroughly examined under conditions of intended use, including the presence of lubricants. Plastics are often mixtures of two or more basic types, and it is difficult to predict the refrigerant's effect. Swelling data can be used as a general guide of effect, but, as with elastomers, the effect on properties of the plastic should also be examined. Extensive test data for compatibility of plastics with refrigerants and lubricants are reported by Cavestri (1993), including 23 plastics, 10 refrigerants, 7 lubricants, and 17 refrigerant/lubricant combinations. Refrigerants and lubricants had little effect on most of the plastics. Three plastics (acrylonitrile-butadiene-styrene, polyphenylene oxide, and polycarbonate) were affected enough to be considered incompatible. In a separate study by DuPont Fluoroproducts, two additional plastics (acrylic and polystyrene plastics) were determined to have questionable compatibility with HCFC and HFC refrigerants.

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^a75 μm film, 100% rh at 38°C. Water diffusion rate is in micrograms per second per square metre of elastomer.

^bFilm thickness = 25 μm; temperature = 25°C. Gas at 101.3 kPa and 0°C. Diffusion rate in cubic centimetres of gas per second per square metre of elastomer.